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Review Article

Measurement and interpretation of the double layer capacitance of Pt(111)/aqueous solution interfaces



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Abstract

The electric double layer (EDL) at Pt(111)/aqueous solution interfaces is, in some sense, a shelter for electrocatalysis, where one can find solace in exploring the fundamentals before venturing into the labyrinthine landscape of real-world intricacies. Although seemingly unpretentious, classical electrochemical methods such as cyclic voltammetry (CV) and electrochemical impedance spectroscopy (EIS) play an indispensable role in quantitative investigation of this EDL. However, these measurements and interpretation are highly nontrivial, and three related issues are addressed in this Opinion article. First, we discuss discrepancies among various measurements of the double layer capacitance $C_{\rm dl}$, and recommend separating $C_{\rm dl}$ from possible pseudocapacitances using EIS. Second, following our recommendation, we examine assumptions and limitations of the Frumkin-Melik-Gaikazyan (FMG) model that is the physical model used to extract Cdl from EIS data in the presence of chemisorption. Thirdly, we compare CV-derived $C_{\rm dl}$ and EIS-derived C_{dl} . We explain why EIS-derived C_{dl} is always positive even for the case where CV-derived $C_{\rm dl}$ assumes negative values due to partially charged adsorbates. We hope this Opinion can facilitate the advent of a converged understanding of the EDL at Pt(111)/aqueous solution interfaces.

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Keywords

Electric double layer, Double layer capacitance, Adsorption impedance, Negative capacitance, Pt(111)/aqueous solution interfaces.

Measurements of C_{dl}

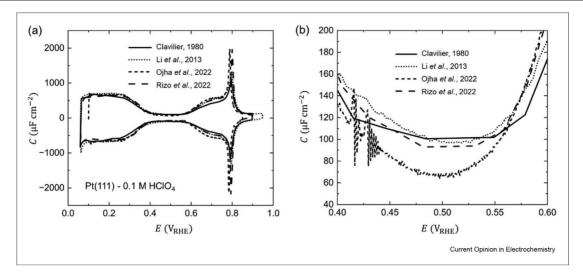
In stark contract with minor fluctuations among the cyclic voltammograms (CV) of Pt(111) in 0.1 M HClO₄ electrolyte solution as documented in previous studies [1–4], the measurements of double layer capacitance ($C_{\rm dl}$) of Pt(111) in similar electrolyte solutions exhibit substantial divergence. This significant discrepancy poses a critical challenge for evaluating the effectiveness of existing double layer models pertaining to these interfaces.

Figure 1(a) displays four CVs in terms of capacitance obtained by dividing the current density by the scanning rate. Small peaks in the hydrogen adsorption/desorption region between $0.05~V_{RHE}$ and around $0.4~V_{RHE}$ are usually attributed to defects on Pt(111), see a recent Opinion [5]. The butterfly peak between $0.55~V_{RHE}$ and $0.9~V_{RHE}$ corresponds to hydroxyl adsorption/desorption [6–8]. The butterfly consists of a prewave and a sharp peak. It is generally accepted that the prewave corresponds to long-range disordered adsorption, and the sharp peak corresponds to phase transition to long-range ordered adsorption [9]. This butterfly peak is incompletely understood, as evidenced by unexpected influence of perchlorate anions on the butterfly [10–12].

The nearly flat, low-lying region from 0.4 V_{RHE} to 0.55 V_{RHE} is assumed to be a pure double layer charging region [8]. Figure 1(b) zooms into this region of Figure 1(a). A variation on the magnitude of 40 μ F/cm⁻² is observed. Moreover, a common capacitance minimum is found at 0.50 V_{RHE} . This capacitance minimum is unlikely the Gouy-Chapman minimum [13] since the potential of zero charge (PZC) of Pt(111) in 0.1 M HClO₄ is around 0.35 V_{RHE} [14,15]. Instead, the capacitance minimum is likely resulted from the transition from the decreasing pseudo-capacitance of hydrogen desorption to the increasing pseudo-capacitance of hydroxyl adsorption as the potential

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Figure 1



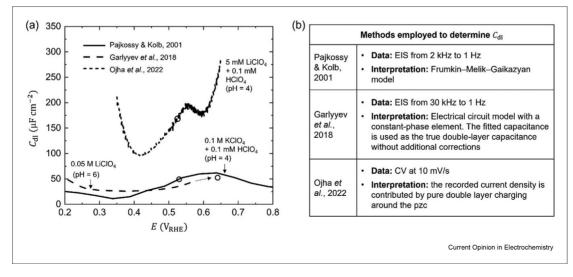
(a) Comparison between cyclic voltammograms of Pt(111)-0.1 M HClO₄ solution interfaces from Clavilier [3] (solid line), Li et al. [4] (short dot line), Ojha et al. [1] (short dash line), and Rizo et al. [2] (dash line). (b) An enlarged view of Figure 1(a) in the double layer region from 0.4 V_{RHE} to 0.6 V_{RHE}.

shifts positive [16]. Shifting the PZC to around 0.5 $V_{\rm RHE}$ requires a solution pH of around 3.

Figure 2(a) shows three curves of the double layer capacitances ($C_{\rm dl}$) in less acidic media measured by three groups using different methods [1,17,18]. No similarity can be found between these results. The earlier $C_{\rm dl}$ from Pajkossy and Kolb has an "S" shape, constituting of an initial decrease up to 0.35 $V_{\rm RHE}$, an increase till 0.6

 V_{RHE} and then a decreasing trend. The recent C_{dl} from Garlyyev et al. is "U" shaped with a low-lying plateau from 0.3 V_{RHE} to 0.45 V_{RHE} . In contrary, a "W"-shaped C_{dl} profile was obtained by Ojha et al. more recently. At such low concentrations of the electrolyte solution, the classical Gouy-Chapman-Stern (GCS) model predicts a camel-shaped C_{dl} profile with the minimum pinpointed at the PZC [13,19]. The deviation from the GCS model has triggered the development of several models for this

Figure 2



(a) Comparison between double layer capacitances ($C_{\rm cl}$) of Pt(111)/aqueous solution interfaces from Pajkossy and Kolb [17] (solid line), Garlyyev et al. [18] (dash line) and Ojha et al. [1] (short dash line). The PZC for each system is calculated by 0.29 + 0.059 pH V_{RHE}, and denoted by the cycles. More details of the methods of determining $C_{\rm cl}$ are listed in (b).

EDL, which has been critically reviewed in a recent Opinion [20].

In addition to variations in shape, the magnitude of $C_{\rm dl}$ also exhibits divergence. According to the GCS model, $C_{\rm dl}$ should decrease in more diluted solutions at the same electrode potential relative to the PZC [13]. However, the experimental data from three different studies do not conform to this theory. The data of Pajkossy and Kolb [17] were obtained in 0.1 M KClO₄ and 0.1 mM HClO₄ solution at pH 4, ranging from 10 to $60 \,\mu\text{F/cm}^2$ as E varies between $0.2 \,\text{V}_{\text{RHE}}$ and $0.8 \,\text{V}_{\text{RHE}}$. Ojha et al. [1] measured C_{dl} in 5 mM LiClO₄ + 0.1 mM HClO₄ with the lowest concentration among the three experiments, is, nevertheless, the highest, ranging from 100 to 300 μ F/cm² as E varies between 0.35 V_{RHE} and $0.65 \, \mathrm{V}_{\mathrm{RHE}}$.

As pointed out recently [16], the discrepancies in shape and magnitude of the C_{dl} profiles could be traced back to different methods employed to determine $C_{\rm dl}$, in addition to inevitable differences in the cleanness of the electrolyte solution. Pajkossy and Kolb extracted $C_{\rm dl}$ from electrochemical impedance spectroscopy (EIS) data in a frequency range of 2 kHz to 1 Hz. The Frumkin-Melik-Gaikazyan (FMG) model was used to separate $C_{\rm dl}$ from the adsorption capacitance $C_{\rm ad}$ [17]. Garlyyev et al. extracted C_{dl} from EIS data in a frequency range of 30 kHz to 1 Hz using an electrical circuit model with a constant-phase element (CPE) [18]. The exponent coefficient n in the CPE is found to be $n = 0.96 \pm 0.01$. Therefore, the fitted capacitance was approximated as the true double-layer capacitance without additional corrections. The $C_{\rm dl}$ from Ojha et al. was calculated from current density recorded in CV measurements. With a deliberate choice of the solution pH in the range between 3 and 4, the PZC falls into the double layer region. They assumed that the recorded current density is contributed solely by pure double layer charging, and the total converted capacitance is believed to be equivalent to $C_{\rm dl}$ [1].

In principle, EIS can separate $C_{\rm dl}$ from possible pseudocapacitances of chemisorption, rendering it the method of choice for $C_{\rm dl}$ measurements [21,22]. The total capacitance C_{total} is reduced to C_{dl} only when the frequency is above a characteristic frequency ω_c based on the FMG model, as to be analyzed in the following section. At low frequencies, $C_{\text{total}}(\omega \rightarrow 0) \approx C_{\text{dl}} + C_{\text{ad}}$, where C_{ad} is the adsorption capacitance. The characteristic frequency ω_c is around 1 MHz for hydrogen adsorption at Pt(111) in 0.5 M perchloric acid [23], and above 10 kHz for hydroxyl adsorption at Pt(111) in 0.1 M perchloric acid [24]. A scanning rate of 10 mV s⁻¹ corresponds to a characteristic frequency below 1 Hz, which is far lower than the typical ω_c of Pt(111) electrode processes. Therefore, it is extremely difficult to separate $C_{\rm dl}$ from $C_{\rm ad}$, if any, in CV measurements.

Albeit being a routine classical electrochemical experiment, accurate measurement of the $C_{\rm dl}$ of Pt/aqueous solution interfaces presents a considerable challenge. As is well known, this is mainly due to the high sensitivity of this interface to minute impurities in the electrolyte solution and a tiny portion of defects on the metal surface. Compared to the linear scanning voltammetry, the alternating cyclic voltammetry seems to better serve the purpose for it allows to filter slow adsorption processes by selecting the frequency [25]. However, it is crucial to establish that the C_{dl} does not change significantly with the applied frequency, as demonstrated in Valette's measurements on silver [26]. Given the likely presence of fast chemisorption processes, we recommend determining $C_{\rm dl}$ from EIS measurements and using a physical model to extract $C_{\rm dl}$. As emphasized in the last section, $C_{\rm dl}$ obtained this way corresponds to a very high frequency. EIS measurements on electrocatalytic interfaces are highly nontrivial. In EIS measurements, it is highly important to be aware of high-frequency artefacts brought by the reference electrode and the measurement system, as elaborated by Tran et al. [27], and to understand the assumptions and limitations of the prevailing physical model - the FMG model, which are discussed below [22].

Extraction of C_{dl} from EIS using Frumkin-Melik-Gaikazyan model

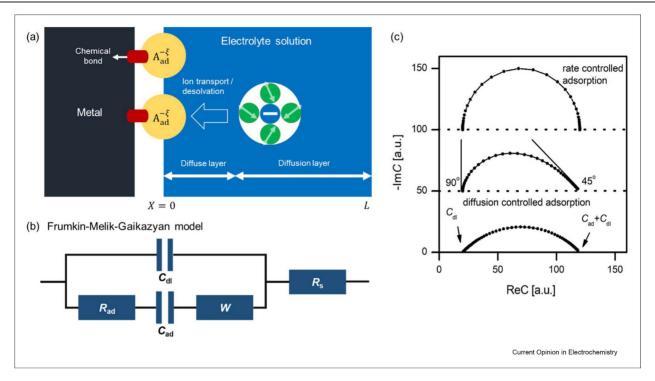
If one employs EIS to determine $C_{\rm dl}$, a proper model is required to extract $C_{\rm dl}$ from the measured EIS data. The appropriateness of the model determines the reliability of the extracted C_{dl} . Therefore, it is crucial to understand the assumptions and limitations of the model used in data analysis.

The FMG model is the physical model for electrocatalytic EDLs with chemisorption [28,29]. The illustration and corresponding FMG model of EDL are shown in Figure 3(a) and (b) [22]. The FMG model describes the chemisorption process using a charge transfer resistance R_{ad} , a pseudo-capacitance of chemisorption C_{ad} , and a diffusion impedance W, which are in series. The double layer capacitance $C_{\rm dl}$ is in parallel connection with the chemisorption branch. In addition, the resistance of the bulk solution R_s is used to describe the ionic conduction in the electrolyte solution. The total capacitance expressed by the FMG model reads,

$$C(\omega) = \frac{1}{j\omega(Z - R_{\rm s})} = C_{\rm dl} + \frac{C_{\rm ad}}{j\omega C_{\rm ad}(R_{\rm ad} + W) + 1}$$
 (1)

where Z is the total interfacial impedance, ω the angular frequency. The diffusion impedance W is often described by the Warburg formula, $W = \sigma_D(j\omega)^{-0.5}$ with σ_D being a coefficient as a function of the diffusion coefficient [30].

Figure 3



(a) The Schematic illustration and (b) the corresponding FMG model describing the electrocatalytic EDL with chemisorption [22]. (c) The capacitance spectra at slow, medium and fast rates of chemisorption, reproduced with permission from Ref. [17]. Copyright, Elsevier.

Figure 3(c) shows the capacitance spectra at slow, medium and fast rates of chemisorption, with the frequency decreasing clockwise [17]. $C(\omega)$ is asymptotic to $C_{\rm dl}$ as $\omega \to \infty$, and to $C_{\rm dl} + C_{\rm ad}$ as $\omega \to 0$ according to Eq. (1). In the intermediate frequency range, $C(\omega)$ is manifested as an arc which becomes more squashed as the diffusion impedance plays a more important role [17,29,31].

The FMG model has several limitations [22]. First, the EDL charging process and the electron transfer process are decoupled, described by $C_{\rm dl}$ and $R_{\rm ad}$, respectively. In reality, electron transfer reactions and EDL charging are intrinsically coupled, which not only impacts the magnitude but also changes the shape of EIS. In a recent work, an inductive loop in low frequency range is ascribed to the aforementioned coupling under nonequilibrium states [32]. Second, both the EDL charging process (C_{dl}) and the mass transport process $(R_{\rm s})$ belong to ion transport in the electrolyte solution but are separately described in the FMG model. Third, $C_{\rm dl}$ is taken as a frequency-independent constant, which is problematic as the EDL charging is an ion transport process which should manifest frequency dispersion [29,33]. At last, the ion transport process is described using the Warburg formula which is limited to pure Fickian diffusion in semi-infinite, dilute electrolyte

solution [34]. These limitations have been addressed in an improved model developed by Huang and Li [22].

Comparison of $C_{\rm dl}$ obtained from EIS and surface free charge density

The above discussion revolves around two different kinds of $C_{\rm dl}$, including $C_{\rm dl}$ determined from EIS, denoted $C_{\rm dl}^{\rm EIS}$, and that from CV, or equivalently, the surface free charge density $\sigma_{\rm free}$, $C_{\rm dl}^{\sigma} = \frac{\partial \sigma_{\rm free}}{\partial E}$ [16]. Table 1 compares the two methods. A striking difference is that while $C_{\rm dl}^{\rm EIS}$ is always positive, $C_{\rm dl}^{\sigma}$ can be negative in the presence of partially negatively charged adsorbed intermediates [16,35].

The difference between $C_{\rm dl}^{\rm EIS}$ and $C_{\rm dl}^{\sigma}$ is due to the hidden fact that they correspond to disparate different frequencies. $C_{\rm dl}^{\sigma}$ obtained from the equilibrium surface charging relation corresponds to a zero frequency. However, when trying to separate $C_{\rm dl}$ from $C_{\rm ad}$ using the FMG model, we actually go to extremely high frequency such that the adsorption and desorption cannot follow up the rapid potential change and do not contribute to the current signal. In this scenario, the origin of negative $C_{\rm dl}$, namely, the change in the chemisorption-induced surface dipoles, is absent at such high frequencies. Therefore, $C_{\rm dl}^{\rm EIS}$ is always positive because it is a structural capacitance. It is worth noting that the frequency

Table 1 Comparison of C_{dl} obtained from two methods.		
Data	EIS	Surface free charge density or CV (if there is no chemisorption)
Method	Fitting EIS data using Eq. (1)	$C_{ m cl} = rac{\partial \sigma_{ m free}}{\partial F}$
Frequency	High enough so that chemisorption does not occur	Zero
Property	Always positive	Could be negative due to adsorbed intermediate with partial negative charge

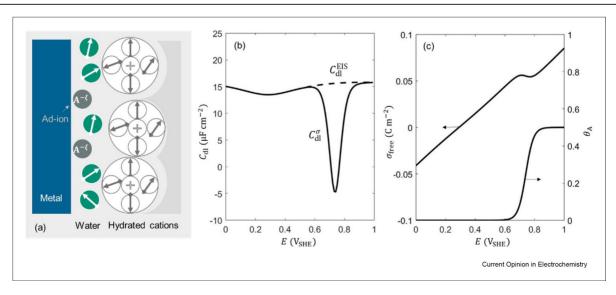
embedded in $C_{
m dl}^{
m EIS}$ is not infinitely high, otherwise even ions cannot move and the resultant $C_{
m dl}^{
m EIS}(\omega o \infty)$ is a pure structural capacitance [36].

Now, we take the Pt(111)-HClO₄ interface as an example to further show the difference between $C_{\rm dl}^{\rm EIS}$ and $C_{\rm dl}^{\sigma}$. Utilizing the EDL model depicted in Figure 4(a) [16], we calculate both $C_{\rm dl}^{\rm EIS}$ and $C_{\rm dl}^{\sigma}$, with details provided in the supporting information. We assume that adsorbed ions A_{ad} have a negative charge of $-0.1 e_0$ and its coverage θ_A increases with the electrode potential as shown in Figure 4(c). The negative charge carried by A_{ad} turns σ_{free} toward more negative values as the coverage increases, leading to negative $C_{\rm dl}^{\sigma}$ until $\theta_{\rm A}$ reaches the maximum. Physical origins of this negative $C_{\rm dl}^{\sigma}$ are referred to a previous Opinion [37]. $C_{\rm dl}^{\rm EIS}$ is calculated using the same model but now the adsorption of ions A does not change at such high frequencies, namely, $\theta_{\rm A}$ is fixed. $C_{\rm dl}^{\rm EIS}$ is always positive and has its minimum at the PZC. Last but not the least, the negative $C_{\rm dl}$ can also be obtained from the impedance model developed by Huang and Li at low frequencies [22], as introduced in the supporting information.

Conclusion

Three questions pertaining to the Pt(111)/aqueous solution interfaces have been discussed. First, significant discrepancies among different measurements of the double layer capacitance have been observed, which could be attributed to variations in the methodologies used to determine $C_{\rm dl}$. We recommend determining $C_{\rm dl}$ from EIS measurements in conjunction with a physical model to eliminate the influence of unintended fast chemisorption processes. Second, the Frumkin-Melik-Gaikazyan (FMG) model has been analyzed in terms of its assumptions and limitations, compared to a modified model developed by Huang and Li [22]. Lastly, we compare $C_{\rm dl}^{\sigma}$ calculated from the surface free

Figure 4



(a) The structure of an electrocatalytic EDL with partially charged adsorbates, reproduced with permission from Ref. [16] (b) The calculated double layer capacitance determined from EIS, denoted $C_{\text{dl}}^{\text{EIS}}$, and that from CV, C_{dl}^{σ} , as well as (c) the calculated surface free charge density, σ_{free} , and the coverage of adsorbed A, θ_A , as a function of the electrode electric potential for the Pt(111)-HClO₄ interface. Model parameters are listed in the supporting information of this article.

charge density and $C_{\rm dl}^{\rm EIS}$ extracted from EIS data in conjunction of a proper model. $C_{\rm dl}^{\rm EIS}$ is always positive, while $C_{\rm dl}^{\sigma}$ could be negative in the presence of negatively charged adsorbates. This discrepancy arises because the latter is obtained only at high frequencies, while the former is an equilibrium quantity that corresponds to a zero frequency. The negative $C_{\rm dl}$ can be inferred from nontraditional measurements of surface charge, e.g., via the laser-induced temperature jump method [14,38].

Declaration of competing interest

The authors declare the following financial interests/ personal relationships which may be considered as potential competing interests: Jun Huang reports financial support was provided by Helmholtz Association of German Research Centres.

Data availability

Data will be made available on request.

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Appendix A. Supplementary data

Supplementary data to this article can be found online at https://doi.org/10.1016/j.coelec.2023.101419.

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